

## Websites

EPA Estimation Program Interface (EPI) Suite. Estimation for octanol–water partition coefficient  $\log K_{ow}$ , Henry's law constant, melting point, boiling point, vapor pressure, water solubility. Requires SMILES notation with help guide.  
<http://www.epa.gov/oppt/exposure/docs/episuite.htm>.

## Exercises

- Develop correlations for the van der Waals attraction term  $a$  and the volume term  $b$ , using the molecular weight as the predictor.
  - Find the values of  $a$  and  $b$  for the following families of compounds: noble gases, period 1 to 6; normal paraffins, 1 to 20 carbon atoms; 1-chloro paraffins, 1 to 10 carbon atoms; 1-alcohols, 1 to 10 carbon atoms.
  - Make graphs of van der Waals  $a$  ( $y$  axis) versus MW ( $x$  axis). How do these four families differ in their intercepts and slopes? Which chemical has the largest slope (most molecular weight dependent), and which chemical has the smallest slope?
  - Make one-parameter linear correlations and compute their  $R^2$  and SD values.
- Make a correlation for the viscosity of R134a in  $\mu\text{Pa s}$ , from  $-50$  to  $+100$  °C in  $10$  °C intervals. (Hint: a possible source of data is NIST Chembook.)
  - Make a linear regression in the form  $\mu = C_0 + C_1T$ . Obtain the coefficients  $C_0$  and  $C_1$ , as well as  $R^2$ ,  $\text{SD}(\mu - \mu')$ , the maximum error, and the maximum percentage error.
  - Make a more accurate quadratic regression in the form  $\mu = C_0 + C_1T + C_2T^2$ . Compare the improvements of the quadratic correlation on the values of  $R^2$ , the standard error, the maximum error, and the maximum percentage error.
  - Make an exponential regression in the form  $\mu = C_0 \exp(C_1T)$ . How does it compare with the two previous correlations?
- The correlations of liquid viscosities with structural and ambient parameters pose difficult problems. Yaws recommended the following equation for the viscosity at  $25$  °C for paraffins:

$$\log_{10}(\mu) = A + B/T + CT + DT^2 \quad T \text{ in kelvin}$$

The recommended parameter values, and the temperature range of validity, are:

- Make plots of viscosity versus temperature in the range  $-50$  °C (coldest winter in North America) to  $250$  °C (hot engine) for these six compounds.

(b) If the  $DT^2$  term is eliminated, how much difference would it make to the results?

	$A$	$B$	$10^2C$	$10^5D$	$Min. T$	$Max. T$
$C_6$	-5.0715	655.36	1.2349	-1.5042	178	507
$C_8$	-5.9245	888.09	1.2955	-1.3596	216	569
$C_{10}$	-6.0716	1017.7	1.2247	-1.1892	243	618
$C_{12}$	-7.0687	1253.0	1.3735	-1.2215	262	658
$C_{14}$	-7.8717	1446.7	1.4940	-1.2495	260	692
$C_{16}$	-8.1894	1557.0	1.5270	-1.2371	291	721

4. The Joule-Thompson coefficient measures the temperature change when a gas is expanded into a vacuum. For the refrigerant R134a, we have the following values:

$Temperature, ^\circ C$	$Joule\text{-}Thomson\ coefficient \times 10^5, K/torr$
-50	-4.19
-40	-3.92
-30	-3.61
-20	-3.24
-10	-2.79
0	-2.26
10	-1.60
20	-0.770
30	0.297
40	1.71
50	3.66
60	6.48
70	10.9
80	18.6
90	35.9
100	109.3

- (a) Make a plot of the Joule-Thompson coefficient versus temperature. What functional form would you suggest that would require the least number of coefficients to achieve the highest value of  $R^2$ ?
- (b) Make the correlation; compute the values of  $R^2$ , standard error, maximum error, and maximum percentage error.